

**Hydrogen, Fuel Cells & Infrastructure Technologies Program  
2004 Annual Review**

Philadelphia, Pennsylvania, May 24-27, 2004

**Direct Methanol Fuel Cells**

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*This presentation does not contain any proprietary or confidential information*

## Selected Collaborations & Commercial Interactions (C)

- **Catalyst Research & Development**

**Johnson Matthey:** Dr. David Thompsett – Pt-Ru catalysts for the anode

**Superior MicroPowders:** Dr. Paolina Atanassova – DMFC MEAs

**E-TEK / de Nora North America:** Dr. Emory de Castro – anode and cathode catalysis

**University of Illinois:** Prof. Andrzej Wieckowski – basic electrocatalysis

**University of New Mexico:** Prof. Plamen Atanassov – non-precious metal catalysis

- **Membranes / Membrane-Electrode Assemblies**

**Virginia Polytechnic:** Prof. James McGrath – alternative polymers and MEAs with significantly improved selectivity and durability

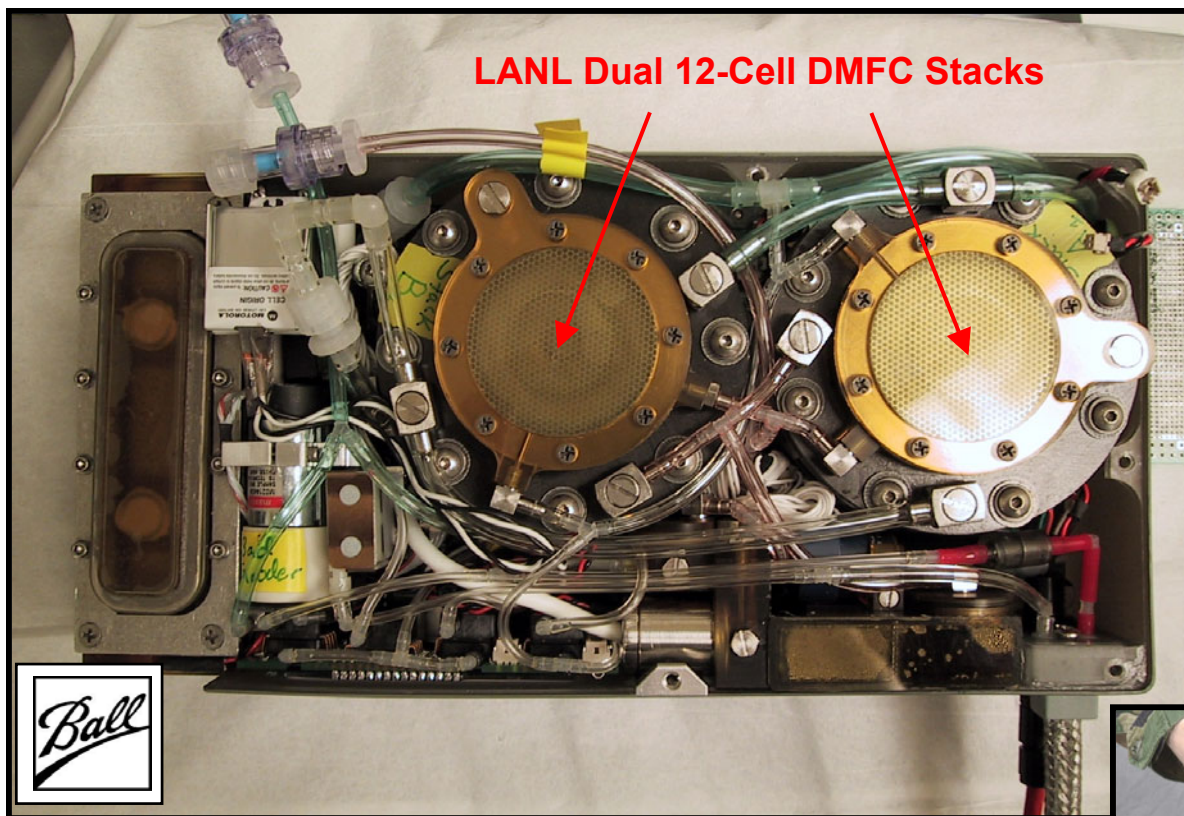
**W. L. Gore:** Dr. Karine Gulati – membranes with improved selectivity

- **DMFC Stacks & Sensors**

**Mesosopic Devices:** Drs. Christine & Jerry Martin – DMFC hardware for portable applications; electrocatalysis

**Ball Aerospace:** Dr. Jeff Schmidt – 20 W portable power system for the military (DARPA Palm Power Program)

# Collaboration with Ball Aerospace (C) Portable Power System for DARPA



## Key System Specs

Rated power:	20 W
Voltage:	12 V
Specific power (72 h mission):	500 W/kg
Efficiency:	33%
Energy yield from fuel:	2 kWh/kg
Converter volume:	1.6 L
Converter weight:	1.6 kg

- LANL DMFC stacks and methanol concentration sensors integrated by Ball Aerospace into first DMFC-20 demonstration units for the military
- Respectable specific power & system efficiency



## DMFC Research: Milestones & FY 2004 Funding

- Determine the impact of Ru crossing on the oxygen reduction kinetics at the DMFC cathode. – *March 2004*
  - Develop methods for synthesis and demonstrate new unsupported DMFC cathode catalyst with average particle size reduced by at least 40% and performance superior to the best commercial cathode catalysts. – *March 2004*
  - Quantify losses in the active surface area of the anode and the cathode over at least 200 h of DMFC operation. – *September 2004*
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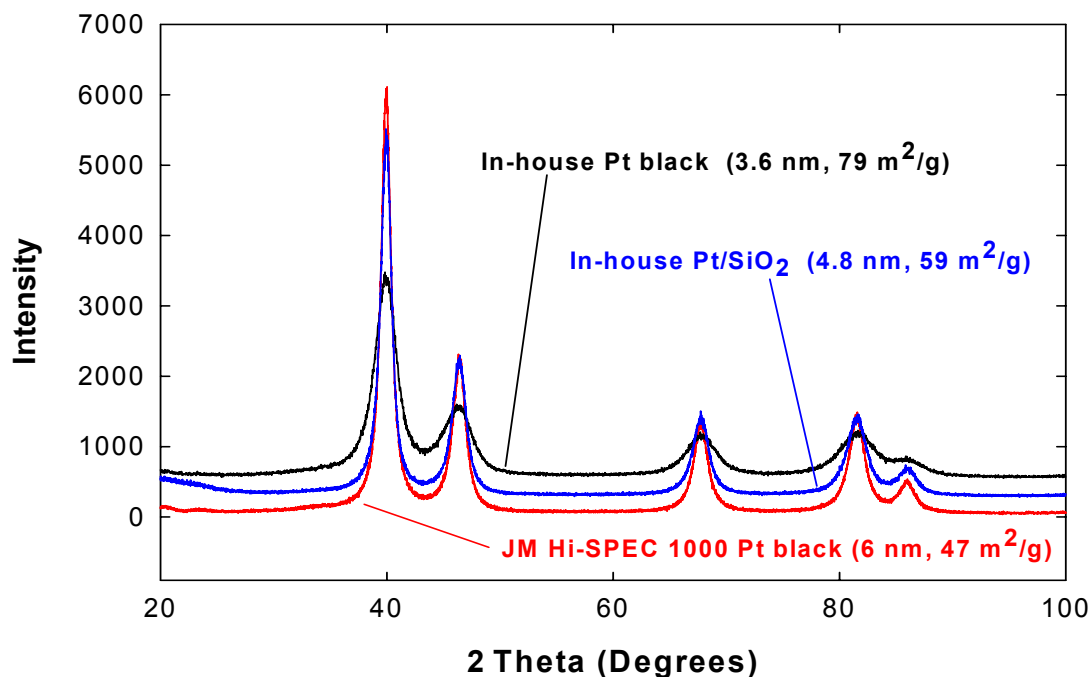
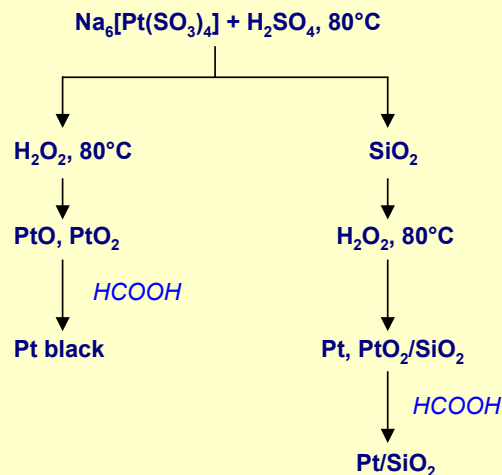
- Total DOE Funding: **\$300 K**

*Irrespective of repeatedly high evaluation scores (3.33 in FY 2003), funding of the LANL DMFC project has been decreased in FY 2004. Reason given: "Technology for portable power applications is near commercialization"; HFCIT Program, FY 2003 Merit Review and Peer Evaluation Report.*

# Electrocatalysis Research

## *Pt Cathode Catalysts with Reduced Particle Size: Approach and XRD Patterns*

### Preparation of Pt black and Pt/SiO<sub>2</sub> Two Approaches

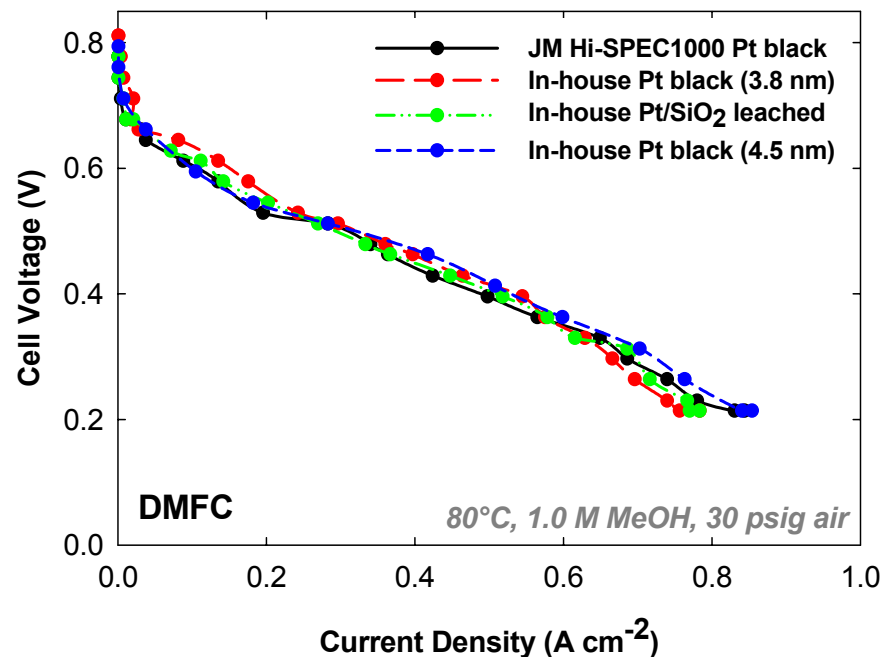
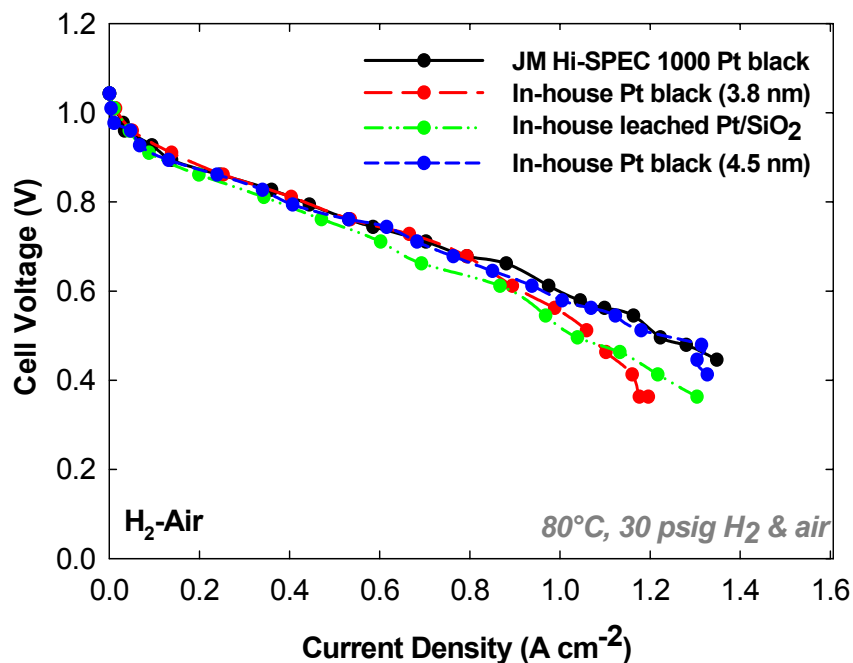


- Average particle size reduced from 6 nm (Johnson Matthey's HiSPEC™ 1000, the state-of-the-art Pt black catalyst for DMFCs) to **3.6 nm** and **4.8 nm**, for Pt black and Pt/SiO<sub>2</sub> catalysts, respectively.

**40% higher dispersion of Pt cathode catalyst achieved (2004 Milestone)**

# Electrocatalysis Research

## *Pt Cathode Catalysts with Reduced Particle Size: Fuel Test Cell Data*

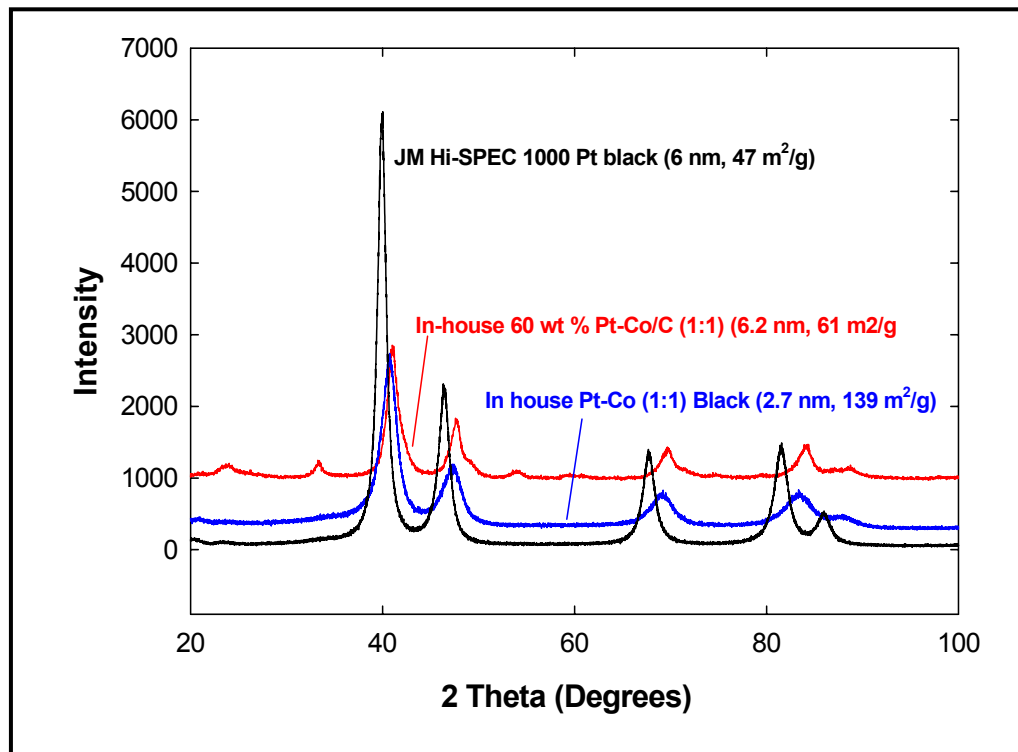


- *Performance of newly synthesized Pt catalysts matches that of the best commercial DMFC cathode catalysts.*
- *Catalyst utilization needs to be improved in order to take full advantage of the smaller particle size of LANL's catalysts.*



# Electrocatalysis Research

## *Pt-Co Binary Cathode Catalysts*



- *Developed two new synthesis approaches for Pt-Co binary catalysts.*
- *High temperature method: Uniquely high metal-loading for Pt-Co/C catalyst (up to 60 wt%) and small average particle size (6.2 nm).*
- *Low temperature method: Very small average particle size of unsupported catalyst (~2.7 nm – 55% particle size reduction relative to HiSPEC™ 1000).*

# Membrane / MEA Research Objectives

## Alternative aromatic hydrocarbon-based membranes for fuel cells:

- ✓ High conductivity, good mechanical properties and chemical stability
- ✓ Low methanol permeability
- ✓ At least an order of magnitude lower cost



Collaboration with  
Virginia Tech

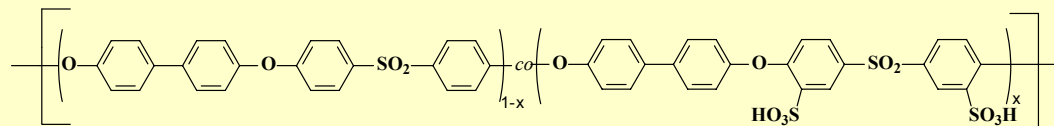
## Key technical issue:

- ✓ Performance loss due to interfacial incompatibility with Nafion-bonded electrode

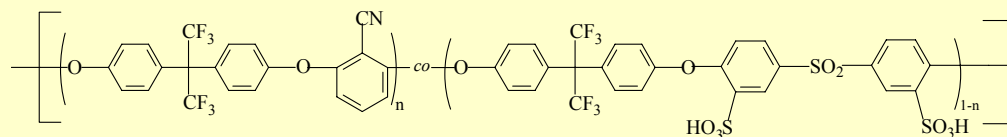
## Research focus

- ✓ Develop membranes compatible with Nafion-bonded electrodes
- ✓ Determine initial and long-term fuel cell performance of MEAs

**BPSH-XX**



**6FCN-XX**

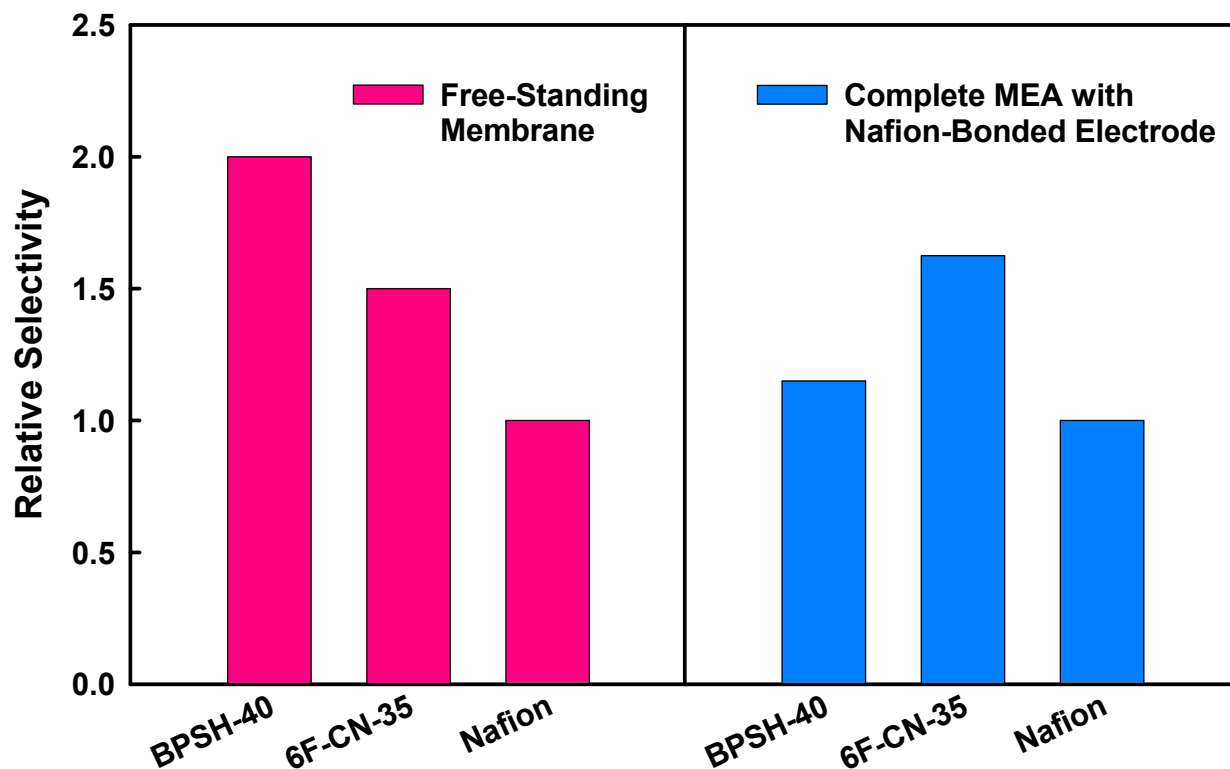


**XX** - percentage of disulfonated monomer units



# Membrane / MEA Research

## Membrane vs. MEA Selectivity



### Membrane Selectivity

Ratio of proton conductivity to methanol permeability

### MEA Selectivity

$$\alpha = \frac{1}{HFR \times \zeta_{\text{lim},n}}$$

HFR = MEA impedance

$\zeta$  = limiting MeOH crossover value (at OCV)

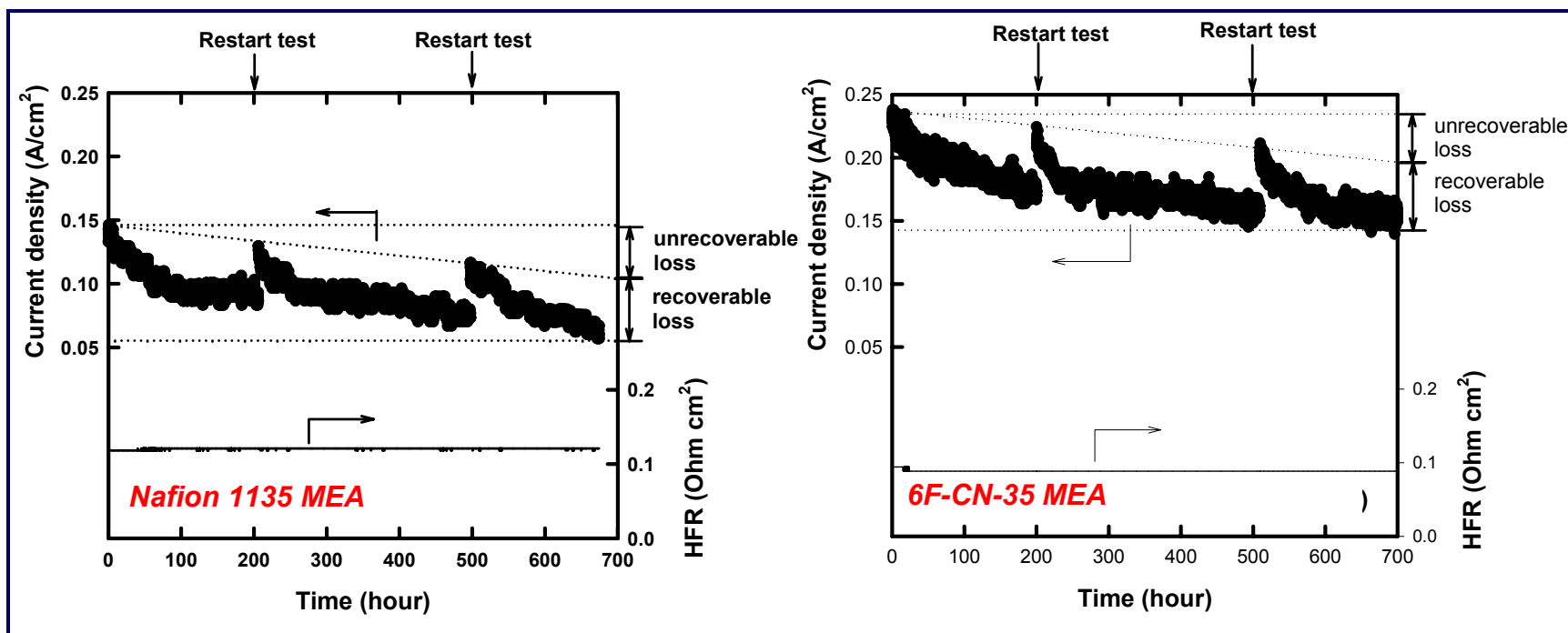
### Relative Selectivity

Membrane-to-Nafion selectivity ratio

- Expected selectivity gains of BPSH-40 not realized in fuel cell testing.
- 6F-CN-35 MEA exhibits **much higher selectivity** than regular Nafion MEA.

# Membrane / MEA Research

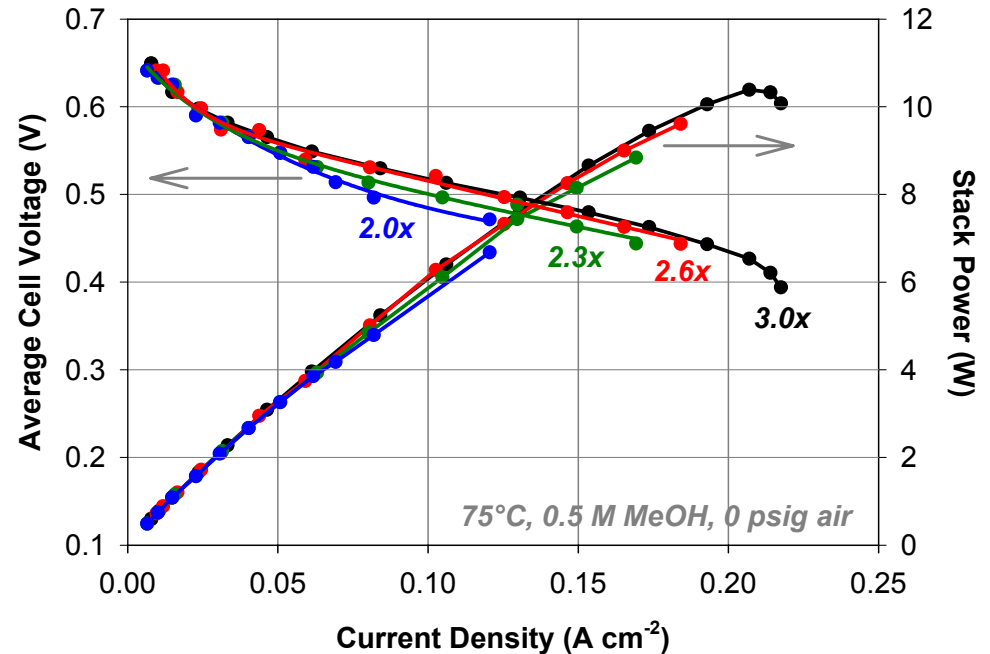
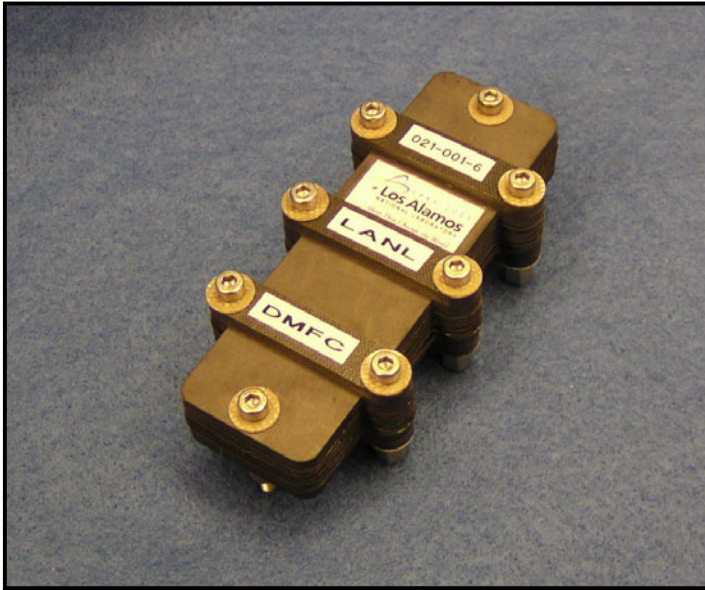
## Performance Durability (80°C, 0.5 V)



- *Good and stable membrane/electrode interface indicated by no change in the resistance of 6F-CN-35 MEA over time.*
- *Similar 700-hour performance losses for 6F-CN-35 and Nafion MEAs*
- *Much higher initial performance of 6F-CN-35 maintained throughout the life test → **significant achievement** in the alternative DMFC membrane research.*

# High Specific-Power Stack for Portable Applications

## Short Six-Cell Stack Testing



**First test of high specific-power stack: (i) uniform operation of individual cells, (ii) very little sensitivity to the air flow, (iii) anode-limited performance.**

**Growing industrial interest; significant technology transfer potential**

**High specific-power stack project currently supported by  
Los Alamos National Laboratory's Technology Maturation Fund**

# High Specific-Power Stack for Portable Applications

## Stack Performance vs. DOE Technical Targets

- Expected maximum specific power of the 25-cell stack: **400 - 500 W/kg**.
- Stack performance promises to exceed DOE's Technical Targets for Consumer Electronics systems for both 2006 & 2010

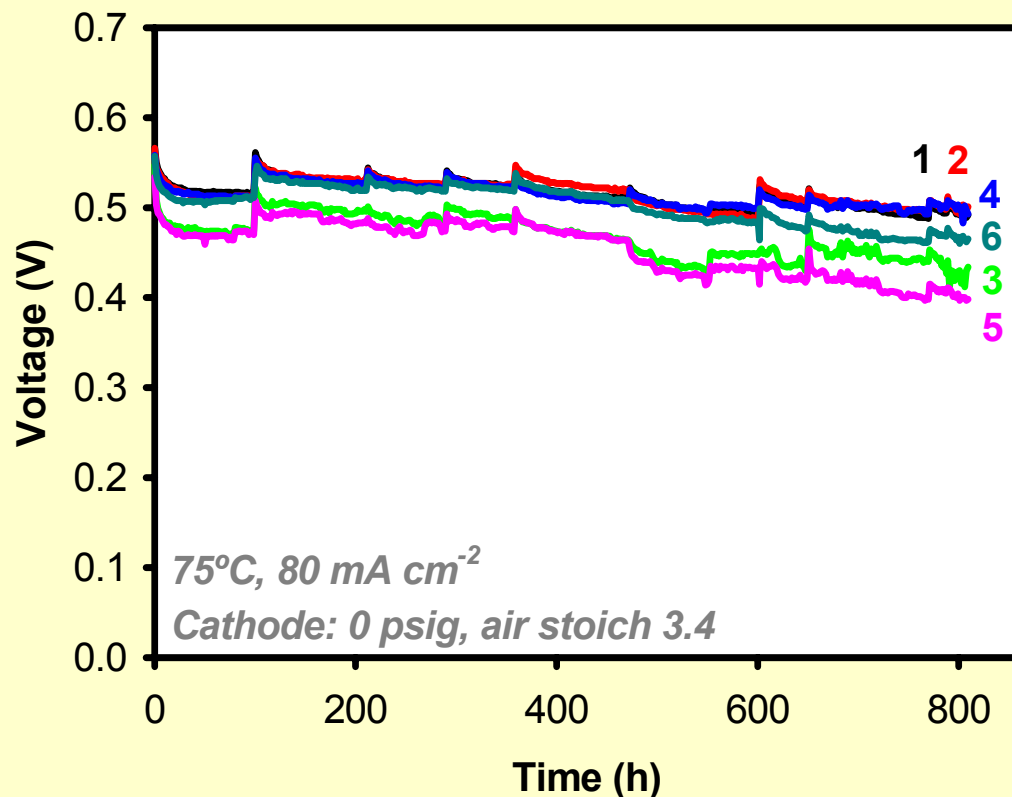
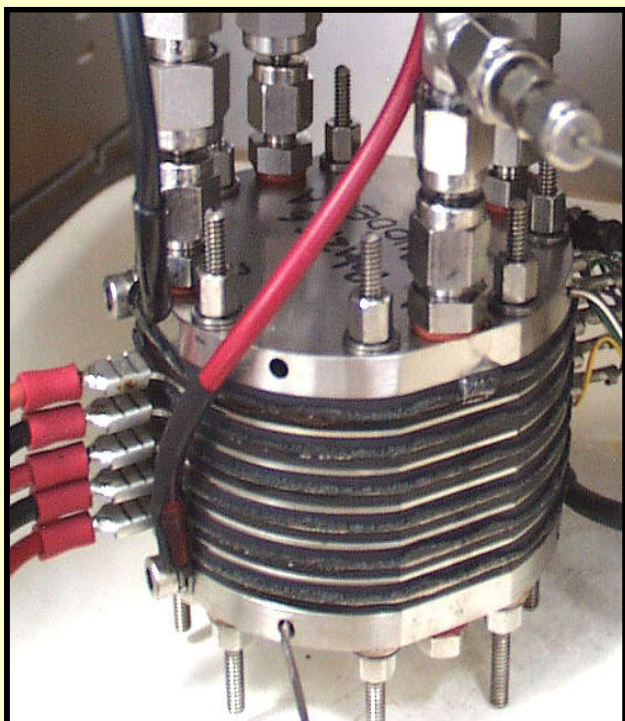
**Table 3.4.7. Technical Targets: Consumer Electronics (sub-Watt to 50-Watt)<sup>a</sup>**

Characteristics	Units	Calendar year		
		2003 status	2006	2010
Specific Power	W/kg	unavailable	30	100
Power Density	W/L		30	100
Energy Density	W-h/L		500	1,000
Cost	\$/W		5	3
Lifetime	hours		1,000	5,000

<sup>a</sup>Few sub-watt to 50-watt fuel cell systems exist and it is premature to specify current status.

## Durability Research

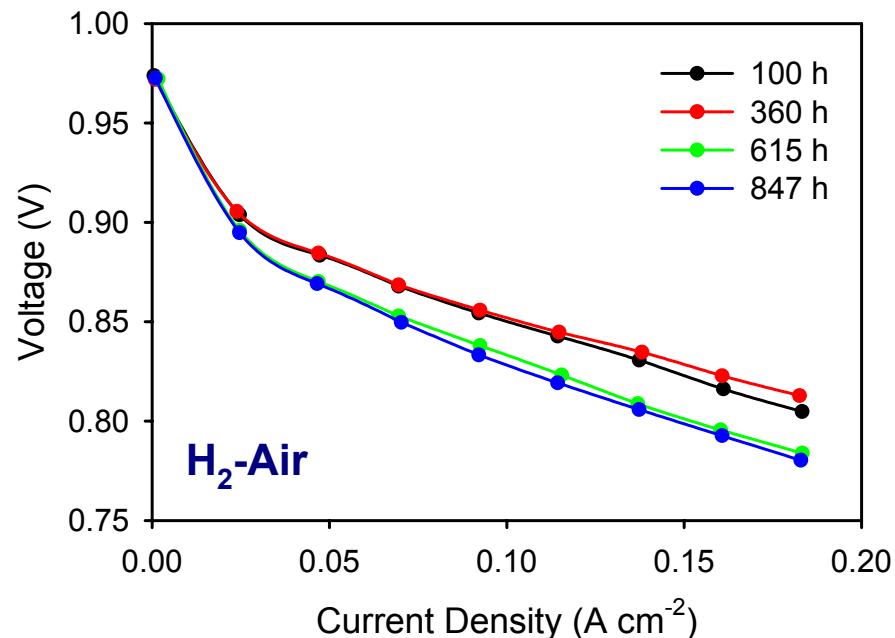
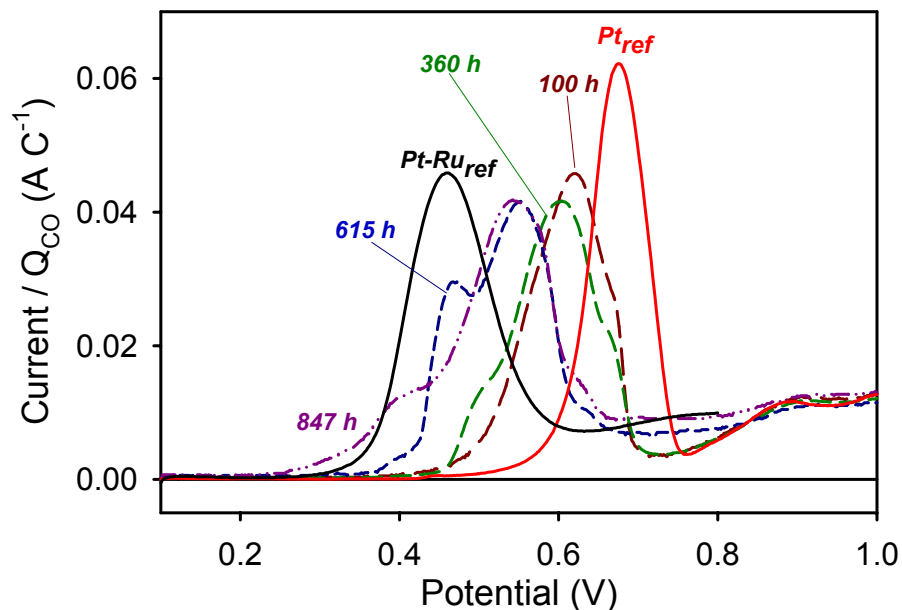
### 850-Hour DMFC Life Test: Possible Causes of Cell Performance Loss



- Surface area loss of the cathode and/or anode catalyst
- Cathode surface oxidation
- Diminished cathode hydrophobicity → “flooding”
- Ruthenium crossover and subsequent accumulation at the cathode

# Durability Research

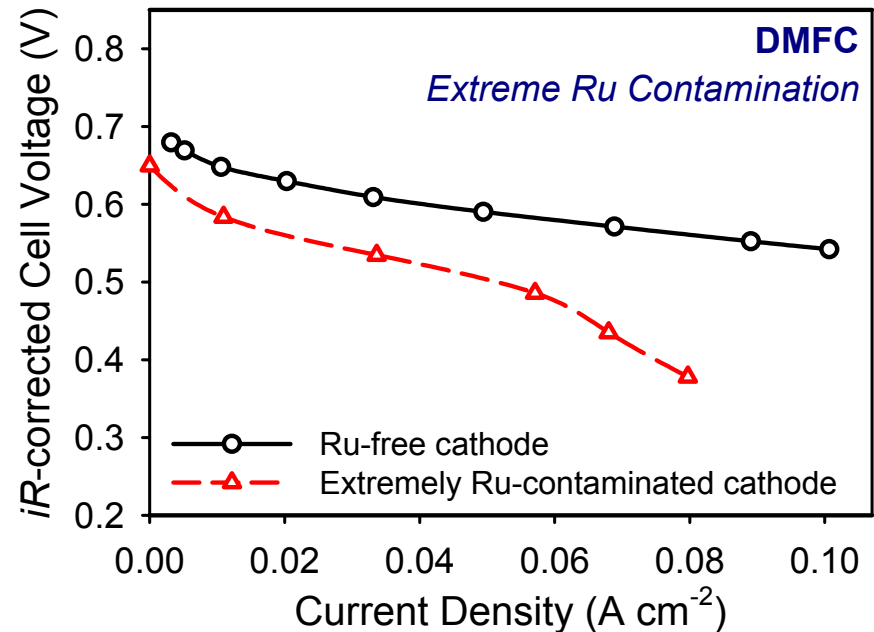
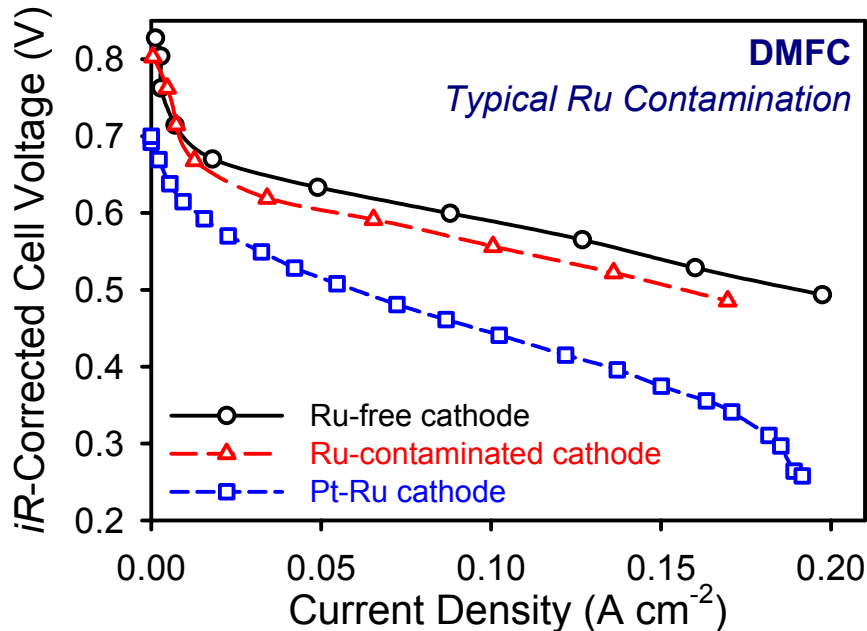
## Ruthenium Crossover: Effect on Oxygen Reduction



- Cathodes in 'typical' DMFCs (Pt-Ru black anode, Nafion<sup>TM</sup> membrane, Pt black cathode) become gradually contaminated by Ru migrating from the anode.
- CO stripping data at different stages of the life test correlate well with the cathode's kinetic performance.
- Oxygen reduction alone is inhibited by Ru crossover by **~25 mV** at  $0.1 \text{ A cm}^{-2}$  after several hundred hours of cell operation.

# Durability Research

## Ruthenium Crossover: DMFC Performance Loss



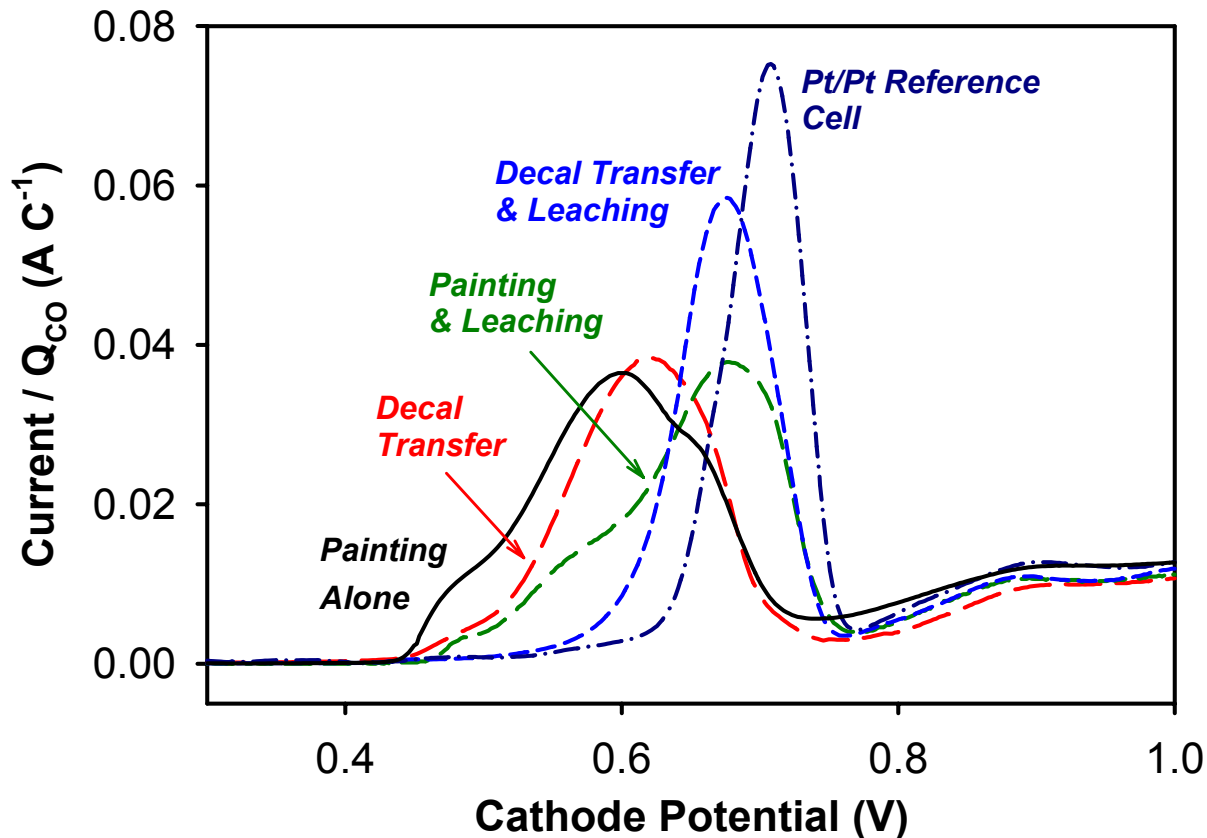
- **Overall DMFC performance penalty resulting from slower oxygen reduction and lower cathode tolerance to crossover methanol: ~40 mV (moderate Ru contamination of the cathode after hundreds of hours of DMFC operation).**
- **Extreme Ru-contamination: ~200 mV cell voltage loss.**

**2004 Milestone Accomplished**



## Durability Research

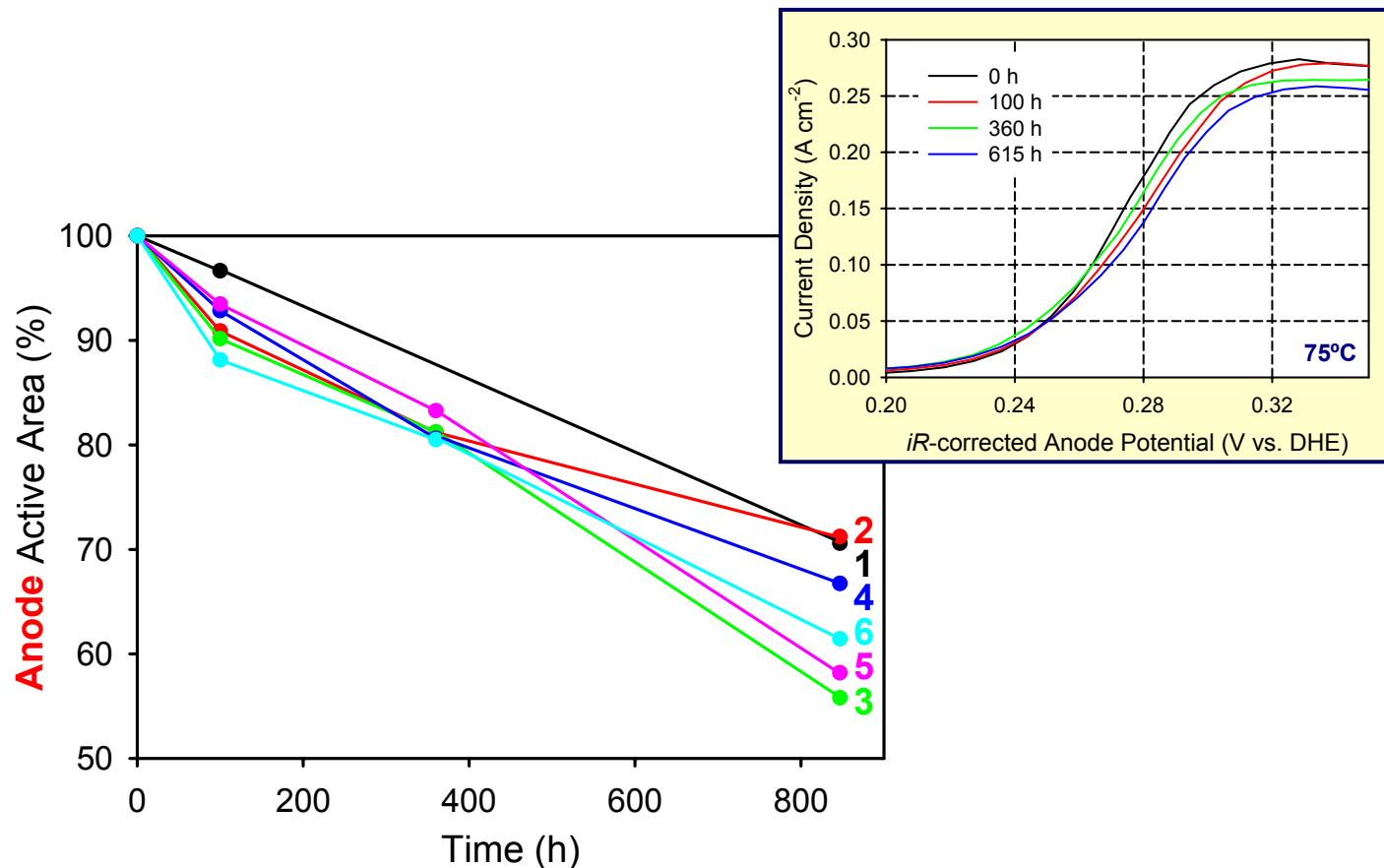
### *Ruthenium Crossover: Preparation of MEAs with “Ru-free” Cathodes*



- Virtually Ru-free cathodes observed following removal of loosely-bound Ru in the anode catalyst & better anode curing (after break-in data; no life-tests performed).***

# Durability Research

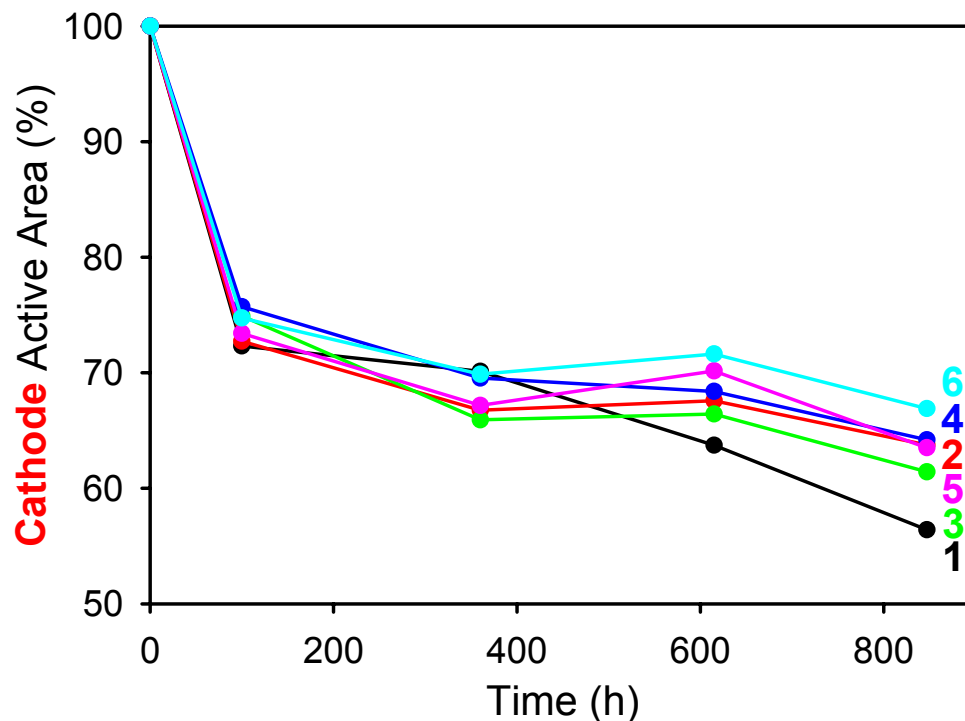
## Loss of Anode Active Surface Area



- **35% - 40% anode surface area loss revealed by CO stripping after 850 hours of cells operation.**
- **Very little impact on DMFC performance.**

# Durability Research

## Loss of Cathode Active Surface Area

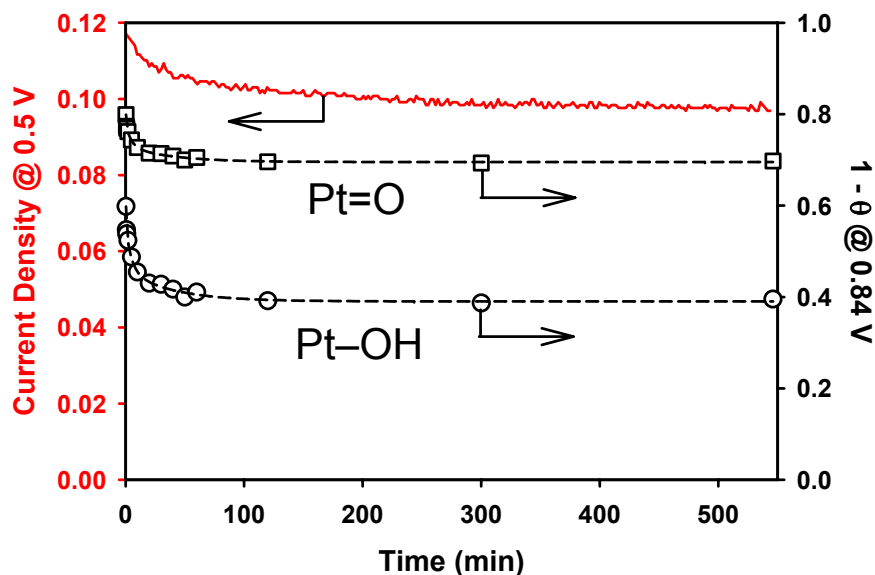


- **35% - 40% cathode surface area loss revealed by CO stripping after 850 hours of cells operation (similar loss as for the anodes).**
- **Possible significant impact on cell performance.**

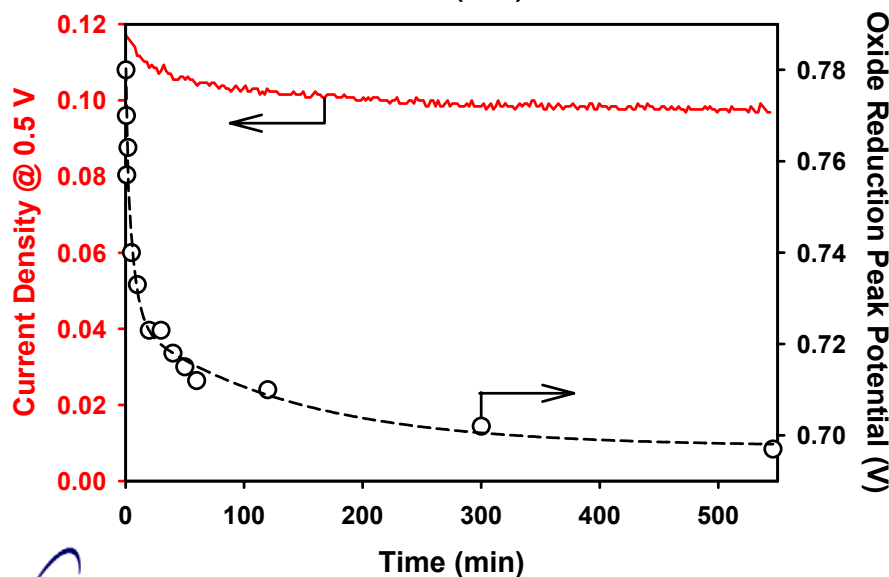
**2004 Milestone Accomplished & Exceeded**

# Durability Research

## Cathode Oxidation vs. DMFC Performance Loss



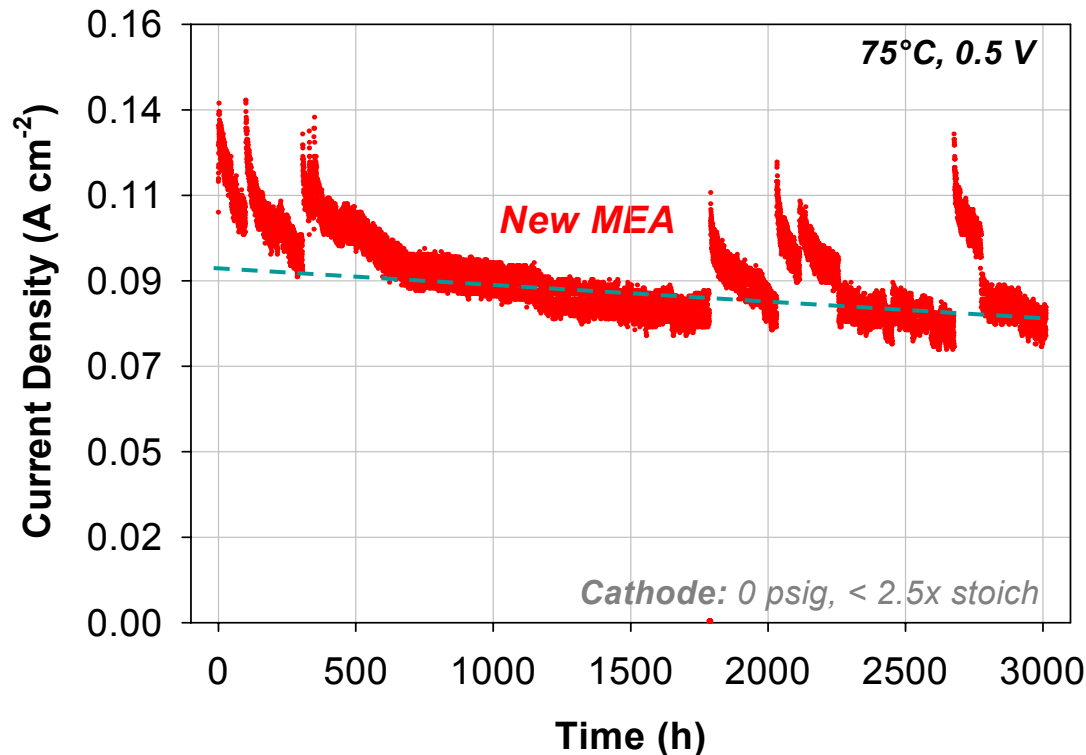
- No obvious correlation observed between the rates of catalytic sites blockage by surface 'OH' and/or 'O' species and DMFC performance loss.
- Based on percent loss of cell performance over time, 'O' is the more likely surface species.



- Transition of the cathode oxide beyond the point of surface coverage saturation is a likely reason for cell performance drop at times longer than two hours ( $\rightarrow$  lessened Pt catalyst activity in oxygen reduction reaction).

# Durability Research

## Novel DMFC MEA with Improved Stability



- New LANL-developed Nafion-based MEA tested for **3000 hours** under challenging conditions of low air “stoich” and ambient cathode pressure.
- 3000-hour performance loss limited to **~12%** (with fully oxidized cathode).

## Technical Accomplishments & Progress (*Highlights*)

### Performance Durability:

- ✓ Determined impact of Ru crossover on DMFC cathode performance (**Milestone #1**); proposed two methods for Ru crossover reduction
- ✓ Quantified anode & cathode surface area losses in the 850-hour life test (**Milestone #3**)
- ✓ Correlated transformation of Pt oxide and cathode performance loss
- ✓ Demonstrated new Nafion-based MEA with performance loss reduced to ~12% over 3000 hours

### Membrane & MEA Research:

- ✓ Demonstrated much higher than Nafion's selectivity of 6F-CN-35 membrane in operating cell
- ✓ Maintained superior performance of the 6F-CN-35 MEA for 700 hours

### Cathode Electrocatalysis:

- ✓ Synthesized in-house Pt and Pt-Co catalysts (unsupported and supported) with significantly reduced average particle size – **Milestone #2's 40% particle-size reduction goal achieved; work will focus on performance**

### High Specific-Power Portable Stack:

- ✓ Designed, built and successfully tested first short six-cell stack

## Selected Reviewers' Comments

**R** *“Astonishing productivity on all key areas of DMFC”*

**R** *“Good balance of theoretical understanding and practical experiments. But why move to higher power?”* Higher power stack effort was abandoned in late FY03. Instead, the project has focused even more on key issues for the future of DMFCs: (i) performance durability, (ii) alternative membrane/MEA development and (iii) cathode operation. Small effort has continued in the high specific-power DMFC stack, the project now internally supported by LANL..

**R** *“Transfer stack making technology to an industrial company”*

A government-use license has been issued to Ball Aerospace for military applications (20 W portable system). Several companies expressed significant interest in the stack, methanol-sensor and novel-MEA technologies. Substantial discussions in progress.

**R** *“Stay with your strengths – focus on improving performance and fundamental understanding”* These have actually been the two main thrust areas of the DMFC research at LANL in FY04.

**R** *“Continue funding”*



## Research Plans

### Remainder of FY 2004

- Determine and optimize performance of new LANL-synthesized highly-dispersed cathode catalysts
- Verify performance stability of novel Nafion-based MEAs, recently life-tested for 3000 hours
- Demonstrate a complete 25-cell high specific-power stack for portable applications

### FY 2005 Objectives *(All key to successful commercialization of DMFCs)*

- Determine impact of changing hydrophilic/hydrophobic properties of the cathode on DMFC performance and performance durability
- Explore introduction of non-precious metal electrocatalysts as means of lowering DMFC cost
- Minimize or altogether eliminate Ru crossover in DMFCs
- Establish materials and techniques allowing consistent fabrication of highly selective and durable alternative MEAs for DMFCs

# DMFC Research: Project Safety

## Administrative Safety Controls

- ✓ **Hazard Control Plan (HCP):** Hazard-based safety review
- ✓ **Integrated Work Document (IWD):** Task-based safety review
- ✓ **Integrated Safety Management (ISM):** Define work → Analyze Hazards  
→ Develop controls → Perform work → Ensure performance

## Engineering Controls

- ✓ **Hydrogen and carbon monoxide laboratory sensors for hydrogen testing (cell break-in, anode polarization testing, surface area determination)**
- ✓ **In the process of replacing tube hydrogen gas storage with on-demand electrolytic hydrogen generators**
- ✓ **Generally low and very low risk operations**

## Potentially Useful DMFC Safety Tip

- ✓ **Direct sink disposal of low-concentration aqueous methanol waste is acceptable after dissolved CO<sub>2</sub> is removed by neutral gas purging and, consequently, initially acidic solution pH increases to neutral.**